Vapor Pressures of Some High Molecular Weight Hydrocarbons

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Vapor pressures, between 5 \times 10⁻⁶ and 10⁻¹ torr., of thirteen hydrocarbons with molecular weights between 220 and 395 have been measured by an effusion method.

THE VAPOR PRESSURES of thirteen hydrocarbons with molecular weights in the range of 220 to 395 were measured by a Knudsen effusion method similar to that used by Bradley and Shellard (2). The hydrocarbon under examination was introduced into a glass bulb in which a small hole had been drilled. The bulb was suspended from the arm of a microbalance which was sensitive enough to detect weight changes of the order of 5×10^{-8} grams. The balance was then connected to a vacuum system and evacuated. The rate of effusion of the hydrocarbon through the hole was determined from rate of loss of weight from the bulb.

Each hydrocarbon was examined successively in six bulbs, the sizes of holes in which varied from 0.025 to 2 mm. diameter. The rates of effusion were so small that the cooling of the bulb by evaporation brought about a temperature change of less than 0.1° C.

The rates at which the hydrocarbon vapors effused were compared with the rates of effusion of the vapor of pure benzophenone from each of the bulbs. The vapor pressures of the hydrocarbon could then be calculated from the known vapor pressures of benzophenone (3). The vapor pressures were independent of the hole size.

The temperature, measured by thermometers sensitive to 0.01° C., was maintained constant to $\pm 0.02^{\circ}$ C. by an oil bath, which surrounded the apparatus.

The hydrocarbons were of high purity, the majority being obtained from API Project 42. They were:

Tricyclopentylmethane ²	$C_{16}H_{28}$
9-Butylanthracene ^a	$C_{18}H_{18}$
1,6-Diphenylhexane	$C_{18}H_{22}$
1,2,3,4,4a,7,8,9,10,11,12,12a-Dodecahydrocrysene ^a	$C_{18}H_{24}$
Perhydrochrysene	$C_{18}H_{30}$
1,6-Dicyclohexylhexane	$C_{18}H_{34}$
Tricyclohexylmethane	$C_{19}H_{34}$
1,1-Dicyclohexylheptane ⁴	$C_{19}H_{36}$
Nonadecane	$C_{19}H_{40}$
1,5-Dicyclohexyl-3-(2-cyclohexylethyl)pentane	$C_{25}H_{46}$
9-Dodecylanthracene ^e	$C_{26}H_{34}$
Heptacosane	$C_{27}H_{56}$
2,2,4,10,12,12-Hexamethyl-7-(3,5,5-Trimethylhexyl)-	
tridecane	$C_{28}H_{58}$
^a Obtained from API Project 42	

At least 1% w of each hydrocarbon was vaporized from the effusion vessel before measurements were made in order to degas and dry it. Observations were continued until a constant reading was obtained; this usually took several hours. When the temperature of measurement was near its melting point special care was taken to see that the hydrocarbon was not partially melted but was either completely solid or completely liquid.

Table I. Experimental Results				
Temp., ° C.	State	Vapor Press., Torr.		
0.0	Liquid	9.72×10^{-5}		
15.4	Liquid	5.38×10^{-4}		
20.7	Liquid	9.78×10^{-4}		
24.6	Liquid	$1.15 imes 10^{-3}$		
42.7	Liquid	$9.22 imes 10^{-3}$		
53.1	Liquid	$2.18 imes 10^{-2}$		
69.7	Liquid	8.89×10^{-2}		
72.8	Liquid	1.29×10^{-1}		
78.0	Liquid	1.68×10^{-1}		
A = -4065	B = 10	0.825 ± 0.076		

Table II. Experimental Results for 9-Butylanthracene,	
C ₁₈ H ₁₈ (M,W, 228.3; M,P, 46.6–47.0° C.)	

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Temp., ° C.	State	Vapor Press., Torr.
20.0	Solid	$3.46 imes 10^{-6}$
30.0	Solid	1.59×10^{-5}
40.0	Solid	6.21×10^{-5}
55.0	Liquid	3.48×10^{-4}
60.0	Liquid	$6.16 imes 10^{-4}$
70.0	Liquid	$1.57 imes 10^{-3}$
75.0	Liquid	$2.10 imes10^{-3}$
95.0	Liquid	1.04×10^{-2}
100.0	Liquid	1.51×10^{-2}
Solid: $A = -4$	5645 B =	13.818 ± 0.133
Liquid: $A = -4$	4382 B =	9.923 ± 0.067

Table III. Experimental Results for 1,6-Diphenylhexane, C18H22(M.W., 238.4)

Temp., ° C.	State	Vapor Press., Torr
20.0	Liquid	3.56×10^{-5}
31.0	Liquid	1.27×10^{-4}
36.0	Liquid	2.16×10^{-4}
46,0	Liquid	5.90×10^{-4}
57.0	Liquid	1.88×10^{-3}
78.0	Liquid	1.35×10^{-2}
82.0	Liquid	1.95×10^{-2}
95.0	Liquid	5.07×10^{-2}
100.0	Liquid	7.73×10^{-2}
		0.010

 $A = -4595; B = 11.197 \pm 0.048$

	Table IV	. Experin	nental R	esults [.]	for	
1,2,3,4,4a,7,8,9,10,11,12,12a-Dodecahydrochrysene,						
C ₁₈ H ₂₄ (M.W., 240.4; M.P., 40.8–41.2° C.)						
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Temp.,	°C. State	Vapor Press., Torr.
20.0	Solid	$6.20 imes 10^{-6}$
25.0	Solid	$1.50 imes 10^{-5}$
30.0	Solid	$3.06 imes 10^{-5}$
35.0	Solid	6.19×10^{-5}
40.0	Solid	1.34×10^{-4}
45.0	Liquid	2.21×10^{-4}
50.0	Liquid	3.81×10^{-4}
55.0	Liquid	5.26×10^{-4}
60.0	Liquid	$9.67 imes 10^{-4}$
70.0	Liquid	$2.35 imes 10^{-3}$
75.0	Liquid	3.97×10^{-3}
80.0	Liquid	$4.94 imes 10^{-3}$
85.0	Liquid	7.32×10^{-3}
Solid:	A = -6029; B =	15.370 ± 0.174

Liquid: A = -4396; $B = 10.165 \pm 0.091$

Table V.	Experimental Results for Perhydrochrysene,
	C ₁₈ H ₃₀ (M.W., 246.6)

Temp., ° C.	State	Vapor Press., Torr.
0.0	Liquid	7.38×10^{-6}
10.0	Liquid	3.05×10^{-5}
20.0	Liquid	8.14×10^{-5}
25.0	Liquid	1.57×10^{-4}
30.0	Liquid	2.70×10^{-4}
40.0	Liquid	$7.74 imes 10^{-4}$
50.0	Liquid	2.02×10^{-3}
55.0	Liquid	3.35×10^{-3}
60.0	Liquid	$4.62 imes 10^{-3}$
70.0	Liquid	1.27×10^{-2}
75.0	Liquid	1.84×10^{-2}
80.0	Liquid	2.94×10^{-2}

 $A = -4298; B = 10.611 \pm 0.162$

Table VI. Experimental Results for 1,6-Dicyclohexylhexane, $C_{18}H_{34}(M.W.,\,250.5)$

Temp., °C.	State	Vapor Press., Torr
15.0	Liquid	$3.25 imes 10^{-5}$
20.0	Liquid	6.21×10^{-5}
30.0	Liquid	1.96×10^{-4}
40.0	Liquid	5.68×10^{-4}
50.0	Liquid	$1.74 imes 10^{-3}$
70.0	Liquid	$9.25 imes 10^{-3}$
100.0	Liquid	1.16×10^{-1}
A = -4474; B =	$= 11.042 \pm 0$.068

Table VII. Experimental Results for Tricyclohexylmethane, C₁₉H₃₄(M.W., 262.5; M.P., 57.3°C.)

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Temp.,	°C. State	Vapor Press., Torr.
28.6	Solid	$6.31 imes 10^{-5}$
36.8	Solid	1.86×10^{-4}
37.7	Solid	$2.38 imes 10^{-4}$
48.0	Solid	1.05×10^{-3}
59.9	Liquid	3.63×10^{-3}
68.2	Liquid	9.30×10^{-3}
70.8	Liquid	1.05×10^{-2}
85.5	Liquid	3.21×10^{-2}
91.6	Liquid	5.05×10^{-2}
Solid: Liquid:	A = -6133; B = A = -4250; B = B	16.096 ± 0.154 10.366 ± 0.126

Table VIII. Experimental Results for 1,1-Dicyclohexylheptane, $C_{19}H_{36}(M.W.,\,264.5)$

Temp., ° C.	State	Vapor Press., Torr
20.8	Liquid	6.55×10^{-5}
25.5	Liquid	1.19×10^{-4}
30.4	Liquid	2.02×10^{-4}
52.3	Liquid	2.23×10^{-3}
68.4	Liquid	9.78×10^{-3}
88.0	Liquid	$5.54 imes 10^{-2}$
95.0	Liquid	8.89×10^{-2}

 $A = -4585; B = 11.416 \pm 0.049$

Table IX. Experimental Results for Nonadecane,
C ₁₉ H ₄₀ (M.W., 268.5; M.P., 32.1°C.)

Temp., ° C.	State	Vapor Press., Torr.
15.0	Solid	4.71×10^{-6}
20.0	Solid	$1.24 imes 10^{-5}$
25.0	Solid	3.23×10^{-5}
30.0	Solid	$7,80 imes 10^{-5}$
33.0	Liquid	1.41×10^{-4}
45.0	Liquid	5.34×10^{-4}
55.0	Liquid	1.57×10^{-3}

Solid: $A = -7135$; $B = 19.430 \pm 0.022$. First order phase transition
at 23°C. [Table 23-2 of API Project 44 (3)] apparently did not
take place during vapor pressure measurement.
<i>Liquid</i> : $A = -4776$; $B = 11.745 \pm 0.043$.

Table X. Experimental Results for
1,5-Dicyclohexyl-3-(2-cyclohexylethyl)pentane,
C ₂₅ H ₄₆ (M.W., 346.6)

Temp., ° C.	State	Vapor Press., Torr
45.0	Liquid	3.45×10^{-6}
65.0	Liquid	3.61×10^{-5}
85.0	Liquid	3.10×10^{-4}
105.0	Liquid	2.28×10^{-3}
125.0	Liquid	1.10×10^{-2}
145.0	Liquid	5.88×10^{-2}

 $A = -5623; B = 12.198 \pm 0.073$

Table XI. Experimental Results for 9-Dodecylanthracene, $C_{\mathfrak{B}}H_{\mathfrak{A}}(M.W.,\ 346.5;\ M.P.,\ 49.5^{\circ}\,C.)$

Temp., ° C.	State	Vapor Press., Torr.
80.0	Liquid	6.25×10^{-6}
90.0	Liquid	2.39×10^{-5}
95.0	Liquid	$5.16 imes 10^{-5}$
105.0	Liquid	1.16×10^{-4}
115.0	Liquid	3.35×10^{-4}
125.0	Liquid	9.86×10^{-4}
130.0	Liquid	1.43×10^{-3}

 $A = -6655; B = 13.692 \pm 0.133$

Table XII.	Experimental Results for Heptacosane,	
C ₂₇ H ₅₆ (M.W., 380.7)		

Temp., ° C.	State	Vapor Press., Torr.
78.1	Liquid	$2.76 imes 10^{-5}$
89.5	Liquid	9.32×10^{-5}
101.0	Liquid	$2.08 imes 10^{-4}$
118.5	Liquid	1.33×10^{-3}
135.4	Liquid	6.27×10^{-3}
161.6	Liquid	5.00×10^{-2}

 $A = -5990; B = 12.441 \pm 0.167$

Table XIII. Experimental Results for 2,2,4,10,12,12-Hexamethyl-7-(3,4,5-trimethylhexyl)tridecane, C₂₈H₅₈(M.W., 394.7)

Temp., ° C.	State	Vapor Press., Torr.
35.0	Liquid	1.50×10^{-5}
45.0	Liquid	5.16×10^{-5}
60.0	Liquid	2.32×10^{-4}
70.0	Liquid	$6.37 imes 10^{-4}$
80.0	Liquid	1.90×10^{-3}
90.0	Liquid	$5.46 imes 10^{-3}$
110.0	Liquid	$2.91 imes 10^{-2}$
120.0	Liquid	$5.56 imes10^{-2}$
A = -5147; B =	11.869 ± 0	.108

The experimental results for each hydrocarbon were a good fit to the equation:

$$\log_{10} P = \frac{A}{T} + B$$

where P is the vapor pressure (torr.), T is the temperature (°K.) and A and B are constants, specific for each hydrocarbon.

The values of A and B for each hydrocarbon were calculated by the method of least squares. The experimental vapor pressures obtained for each hydrocarbon together with the values of the two constants (with a confidence limit at the 95% level) are given in Tables I-XIII.

Vapor pressures reported here are in good agreement with values for higher temperatures published by API Project 4 (1). This is illustrated for one hydrocarbon in Figure 1.

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Figure 1. Vapor pressure of 2,2,4,10,12,12-hexamethyl-7-(3,5,5-trimethylhexyl)tridecane

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A Method for Determining the Solubility of Gases in Relatively Nonvolatile Liquids

Solubility of Methane in *n*-Decane

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H REQUENTLY, industrial operations require knowledge of the solubility of a permanent gas in an essentially nonvolatile liquid. A knowledge of the phase behavior of binary systems consisting of components of widely differing boiling points is essential in the chromatographic study of vapor-liquid equilibria (2, 7). An experimental technique for obtaining such information has been developed and applied to the methane-*n*-decane binary system.

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EXPERIMENTAL APPARATUS

A schematic diagram of the equipment used in this study is presented in Figure 1.

The equilibrium vessel was made of nonmagnetic 304 stainless steel $18\frac{1}{4}$ inches in length, 1.213 inches outside diameter, and 0.750 inch inside diameter. The lower end was closed and the upper end sealed to high pressure by means of an O-ring design (2). A $\frac{5}{8}$ -inch diameter ball bearing was placed within the vessel and used to equilibrate the mixture by raising and lowering a strong horseshoe magnet fitted directly around the cylinder body.